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FR 2805543**ABSTRACT**

L1 ANSWER 1 OF 1 WPIX COPYRIGHT 2004 THOMSON DERWENT on STN
AN 2001-129394 [14] WPIX
CR 2001-073431 [09]
DNC C2001-039053
TI Production of base oil from hydrocarbon charging material, involves performing simultaneous hydrogenation and isomerization of charging material and contact deparaffination of the effluent under specific conditions.
DC H04 H07 K07
IN BENAZZI, E; CSERI, T; GUERET, C; MARCHAL-GEORGE, N; MARION, P; MARCHAL, G
PA (INSF) INST FRANCAIS DU PETROLE
CYC 6
PI JP 2000345170 A 20001212 (200114)* 15 C10G045-62
CZ 2000001568 A3 20010314 (200117) C10G045-62
NL 1015036 C2 20010212 (200121) C10G045-62
KR 2000071874 A 20001125 (200131) C10G049-02
FR 2805543 A1 20010831 (200153) C10G069-02
ES 2185445 A1 20030416 (200335) C10G047-14
ADT JP 2000345170 A JP 2000-132785 20000501; CZ 2000001568 A3 CZ 2000-1568 20000428; NL 1015036 C2 NL 2000-1015036 20000427; KR 2000071874 A KR 2000-23055 20000429; FR 2805543 A1 FR 2000-2364 20000224; ES 2185445 A1 ES 2000-1084 20000427
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IC ICM C10G045-62; C10G047-14; C10G049-02; C10G069-02
ICS B01J023-42; B01J029-068; B01J029-67; C10G007-00; C10G035-085; C10G035-095; C10G045-02; C10G045-64; C10G065-00; C10G065-04; C10G067-02; C10G071-00; C10G073-02
AB JP2000345170 A UPAB: 20030603
NOVELTY - The method involves performing simultaneously hydrogenation and isomerization of charging material containing n-paraffin using a catalyst (I), and contact deparaffination of effluent using a second catalyst (II). Both the steps are performed at specific conditions.
DETAILED DESCRIPTION - The method involves performing:
(a) simultaneously hydrogenation and isomerization of charging material containing n-paraffin using a catalyst (I) containing noble metals precipitated on amorphous acid support; and
(b) contact deparaffination of the effluent from step (a).
The charging material contains less than 1000 ppm of sulfur, less than 200 ppm of nitrogen, less than 50 ppm of metal and 0.2 wt.% or less of oxygen. Step (a) is performed in the presence of hydrogen at 200-500 deg. C, a pressure of 2-25 MPa and a space velocity of 0.1-10/hour. The distribution of noble metal in the first catalyst (I) is 20-100%. Step (b) is performed at 200-500 deg. C, a pressure of 1-25 MPa, a space velocity of 0.05-50/hour and in the presence of a second catalyst (II) containing molecular sieve and hydrogenation-dehydrogenation component, and 50-2000 l of hydrogen per liter of effluent.
USE - For production of base oil used as a lubricant for motor vehicles.
ADVANTAGE - The base oil has good intermediate distillate, high viscosity index, good UV stability and low pour point. The lubricant has good properties.
Dwg.0/3
FS CPI
FA AB
MC CPI: H04-E08; H04-E11; H04-F02A; H04-F02E; K07-A; N01-D02; N02-F02